

## Thermal Decomposition of Peroxyacetyl Nitrate in the Presence of O<sub>2</sub>, NO<sub>2</sub> and NO

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**Summary.** The thermal decomposition of pure *PAN* in N<sub>2</sub> as well as in the presence of added O<sub>2</sub>, NO<sub>2</sub> and NO was studied at 1 atm pressure. In addition to methyl nitrate, NO<sub>2</sub> was a significant N-product of pure *PAN* in N<sub>2</sub> thermal decomposition. In the presence of sufficiently large amounts of O<sub>2</sub>, no methyl nitrate was formed at 333 K, indicating that the homolytic *PAN* decay to methyl nitrate and carbon dioxide is not occurring. In the presence of NO (in contrast to former studies) methyl nitrite was found to be the major organo-nitrogen compound instead of methyl nitrate. The system *PAN*–NO–N<sub>2</sub> allowed the determination of the rate constant  $3.1 \cdot 10^{-4} \text{ s}^{-1}$  at 298 K for reaction (1): *PAN* → CH<sub>3</sub>COO<sub>2</sub> + NO<sub>2</sub>, in agreement with prior studies. Computer simulations based on the free radical mechanism starting with reaction (1) fitted very well the experimental results.

**Keywords.** *PAN*; Thermal decomposition; O<sub>2</sub>; NO<sub>2</sub>; NO.

### Die thermische Zersetzung von Peroxyacetylnitrat in Gegenwart von O<sub>2</sub>, NO<sub>2</sub> und NO

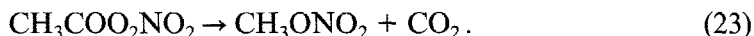
**Zusammenfassung.** Die thermische Zersetzung von reinem *PAN* in N<sub>2</sub> und in Gegenwart von zuge-mischtem O<sub>2</sub>, NO<sub>2</sub> und NO wurde bei 1 atm Druck untersucht. Zusätzlich zu Methylnitrat war NO<sub>2</sub> ein signifikantes N-Produkt bei der thermischen Zersetzung von reinem *PAN* in N<sub>2</sub>. In Gegenwart genügend großer Mengen von O<sub>2</sub> wurde bei 333 K kein Methylnitrat gebildet. Dies zeigt an, daß der homolytische Zerfall von *PAN* zu Methylnitrat und Kohlendioxid nicht eintritt. Im Gegensatz zu früheren Untersuchungen wurde in Gegenwart von NO nicht Methylnitrat, sondern Methylnitrit als wichtigste Organo-Stickstoff-Verbindung gefunden. Im System *PAN*–NO–N<sub>2</sub> wurde die Geschwindigkeitskonstante, in Übereinstimmung mit früheren Untersuchungen, zu  $3.1 \cdot 10^{-4} \text{ s}^{-1}$  bei 298 K für die Reaktion (1): *PAN* → CH<sub>3</sub>COO<sub>2</sub> + NO<sub>2</sub> bestimmt. Computersimulation auf Basis des freien Radikal-Mechanismus beginnend mit Reaktion (1) waren mit den experimentellen Resultaten in sehr guter Übereinstimmung.

### Introduction

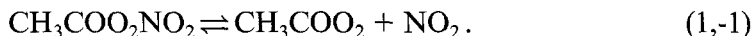
It is now well established that *PAN* is ubiquitous in the atmosphere. It constitutes a significant compound of photochemical smog in the urban areas all over the world, where it may also be used as an index of photochemical air pollution next to ozone. In clean atmospheres *PAN* has been found to be a significant odd nitrogen reservoir [1].

Since the pioneering work of Stephens and coworkers *PAN* is known to decompose thermally with the two major products being methyl nitrate and carbon

dioxide. These products were proposed to be formed by homolytic decomposition of *PAN* via a six-membered cyclic intermediate [2], reaction (23):



Several years later Cox and Roffey [3] and Hendry and Kenley [4] proposed a free radical mechanism starting with reaction (1):



The work of Bruckmann and Willner a few years later corroborated that the free radical was the exclusive mechanism of *PAN* thermal decomposition [5]. Recently however, Senum and coworkers proposed that parallel to the free radical mechanism the thermal decomposition of *PAN* is effected by a homolytic pathway [6]. In the most recent study of *PAN* by Wangberg et al. [7], the heterogeneous factors that affect the *PAN* thermal destruction were studied. These authors could not differentiate between the free radical only mechanism and the homolytic plus free radical mechanism proposed by Senum et al. [6]. They reported that reaction (1) is not effected heterogeneously.

In addition to the above differences on the mechanism, a number of discrepancies still exist on the identity and quantity of *PAN* thermal decomposition products. Thus  $\text{NO}_2$  (which we find to be a significant product of the pure *PAN*/ $\text{N}_2$  decomposition) was not observed at all in many previous studies [6, 7] whereas Bruckmann and Willner [5] reported qualitatively on the  $\text{NO}_2$  formation. Furthermore nitromethane [5, 6] and methyl nitrite [8] were also reported to be products of the pure *PAN* decay without convincing mechanistic explanation. Large discrepancies also exist in the literature in the amounts of methyl nitrate formed from the decay of pure *PAN* [5–7]. Similarly the organo-nitrogen decay products of *PAN* in the presence of  $\text{NO}$  were also not satisfactorily documented in earlier studies [6, 7].

The purpose of the present work was to examine the significance of the homolytic *PAN* destruction as proposed by Senum et al. compared to the free radical mechanism. Because of the uncertainty in the reported reaction products and their quantitative relationships we studied the products formed under a variety of conditions. Thus using ppbv concentrations, so that extrapolations to ambient conditions would be more reliable, we studied the *PAN*– $\text{N}_2$  system as well as the effect of added  $\text{O}_2$ ,  $\text{NO}_2$  and  $\text{NO}$  on the rate of *PAN* decomposition and we obtained quantitative relationships of the products formed.

## Experimental Part

All experiments were carried out at 1 atm pressure using  $\text{N}_2$  as matrix, in a 4.5 l glass flask, equipped with two septa ports and a teflon stopcock and thermostated in an oil bath at  $50 \pm 0.1^\circ\text{C}$ . This vessel was connected to a vacuum line provided with teflon stopcocks. The experiments with  $\text{NO}$  were carried out in a 425 l glass chamber, thermostated at  $23.5 \pm 0.5^\circ\text{C}$ .

*PAN* was prepared starting with the anhydride of acetic acid via peracetic acid [9] which in turn was nitrated to *PAN* according to the procedure of Gaffney et al. [10]. *PAN* was stored in different small vials at  $-10^\circ\text{C}$  and only one portion was removed from each vial when needed after thawing, in order to avoid its decomposition. Freshly prepared *PAN* was always used and thus the peak of methyl nitrate in the *PAN* introduced in the reaction vessels was negligible. Methyl nitrate [11] and methyl nitrite [12] were synthesized by modification of standard methods. The  $\text{NO}$  used, of purity

99.8%, was obtained from Messer Griesheim and was used as such.  $\text{NO}_2$  was prepared daily in darkened glass flasks from  $\text{NO}$  and a 9:1 excess of high purity  $\text{O}_2$ . The pressure measurements were made using MKS Baratron capacitance manometers.

*PAN*,  $\text{CH}_3\text{ONO}_2$  and  $\text{CH}_3\text{ONO}$  analyses were carried out by injecting 0.5 ml samples using gas tight syringes provided with teflon plungers, into a Hewlett-Packard 5890 A gas chromatograph equipped with a  $^{63}\text{Ni}$  electron capture detector and in a Shimadzu Series 8 GC also equipped with a  $^{63}\text{Ni}$  electron capture detector. For the separation of *PAN* and  $\text{CH}_3\text{ONO}_2$  a HP-1, 5-m-long fused silica cross-linked methyl silicone gum column was used, 0.53 mm i.d., 2.65  $\mu\text{m}$  film thickness [13]. When better resolution of methyl nitrate from the air peak was desired a HP-17 column was used, 10-m-long fused silica cross-linked methyl-phenyl silicone, 0.53 mm i.d., 2.65  $\mu\text{m}$  film thickness. Under our operating conditions *PAN* eluted in 2.55 and 3.10 min and methyl nitrate in 0.85 and 1.10 min in the HP-1 and in the HP-17 columns, respectively. Helium was the carrier gas and 10%  $\text{CH}_4/\text{Ar}$  the make-up gas. Methyl nitrite was separated on a 45 cm long glass column, 2 mm i.d. filled with Porapak Q (80/100 Mesh). The use of the Porapak Q column was necessary because the methyl nitrite was not well resolved from the air peak (seen on the ECD) with the HP-1 wide bore column. On the Porapak Q column methyl nitrite was the only eluting compound at 3.25 min. The ovens in both chromatographs were set at 30°C and the HP ECD was operated at 45°C, whereas the Shimadzu ECD was operated at 30°C. The calibration of the ECD's for *PAN*, methyl nitrate and methyl nitrite was carried out using a Pye Unicam GC equipped with a home built  $\text{NO}_x$  chemiluminescence detector, after their conversion to  $\text{NO}$  on a Mo-converter operated at 320°C. The  $\text{NO}_x$  detector could easily be calibrated with standard  $\text{NO}$ . In addition for the analyses of *PAN*, the ECD's were also calibrated against an ion chromatograph after hydrolysis of *PAN* in an alkaline solution and determination of  $\text{NO}_2^-$ -formed.

$\text{NO}$  was determined by its chemiluminescence reaction with ozone. This home built detector was operated at flows 30 ml/min and had a detection limit of 3 ppbv. Unfortunately *PAN*, methyl nitrate, and methyl nitrite were all converted on the Mo-converter to  $\text{NO}$  with 100% efficiency and therefore they contributed 100% to the signal in the  $\text{NO}_2$  mode. Although the concentrations of *PAN*,  $\text{CH}_3\text{ONO}_2$ , and  $\text{CH}_3\text{ONO}$  were known from their determination with the ECD, and thus their contribution to the  $\text{NO}_2$  signal of the  $\text{NO}_x$  detector could be subtracted, still the accuracy in the determination of the  $\text{NO}_2$  concentration was low ( $\pm 30\%$ ) especially when *PAN* and methyl nitrate were high and  $\text{NO}_2$  low.

## Results and Discussion

Our system was simulated by a 23 reaction mechanism shown in Table 1 using the FACSIMILE software. Although for the sake of completeness the complete set of reactions of  $\text{OH}$ ,  $\text{HO}_2$ , and other radicals could have been included in the reaction scheme, computer simulations showed that these reactions had no effect on the measured reactants and products and thus they were omitted.

The rate constant used for reaction (1) at 25°C was determined in this work. The corresponding value at 50°C was obtained from the Arrhenius expression of Schurath and Vipprecht [14] multiplied by the ratio of our rate constant at 25°C versus their rate constant at 25°C. The most of the rate constants were obtained from the most recent literature survey available [15]. The rest of the rate constants were obtained from other recent references [16–20]. For those reactions found in their fall off region at 1 atm pressure, the appropriate second order rate constants were calculated using Troe's expression. The literature rate constants were used as reported and no attempt was made to adjust them in order to fit our experimental data.

In addition to the gas phase reactions the heterogeneous removal of *PAN* and peroxy acetyl radicals was also found by computer simulations to be of great

**Table 1.** Reactions (1)–(22); units  $\text{cm}^3/\text{mol s}$  and  $\text{s}^{-1}$ 

Reaction no.	Simulation Mechanism Reaction	Rate Constants		References
		50°C	25°C	
(1)	$PAN \rightarrow CH_3COO_2 + NO_2$	$9.6 \cdot 10^{-3}$	$3.1 \cdot 10^{-4}$	[14], this work
(-1)	$CH_3COO_2 + NO_2 \rightarrow PAN$		$7.0 \cdot 10^{-12}$	[15]
(2)	$2 CH_3COO_2 \rightarrow 2 CH_3 + 2 CO_2 + O_2$		$2.8 \cdot 10^{-12} \cdot 10^{230/T}$	[15]
(3)	$CH_3 + O_2 (+M) \rightarrow CH_3O_2$	$8.0 \cdot 10^{-13}$	$8.8 \cdot 10^{-13}$	[15]
(4)	$2 CH_3O_2 \rightarrow 2 CH_3O + O_2$	$1.2 \cdot 10^{-13}$	$1.4 \cdot 10^{-13}$	[15]
(5)	$2 CH_3O_2 \rightarrow HCHO + CH_3OH + O_2$		$2.0 \cdot 10^{-13}$	[15]
(6)	$2 CH_3O_2 \rightarrow CH_3OCH_3 + O_2$	$3.3 \cdot 10^{-14}$	$4.0 \cdot 10^{-14}$	[15]
(7)	$CH_3CO_3 + CH_3O_2 \rightarrow CH_3 + CO_2 + CH_3O + O_2$	$1.8 \cdot 10^{-9} \cdot 10^{-781/T}$		[16]
(8)	$CH_3CO_3 + CH_3O_2 \rightarrow CH_3CO_2H + HCHO + O_2$	$4.1 \cdot 10^{-15} \cdot 10^{912/T}$		[16]
(9)	$CH_3O + O_2 \rightarrow HCHO + HO_2$	$7.2 \cdot 10^{-14} \cdot 10^{-469/T}$		[15]
(10)	$CH_3CO_3 + HO_2 \rightarrow CH_3CO_3H + O_2$	$1.0 \cdot 10^{-13} \cdot 10^{577/T}$		[17]
(11)	$CH_3O + NO_2 \rightarrow CH_3ONO_2$	$1.4 \cdot 10^{-11}$	$1.1 \cdot 10^{-11}$	[15]
(12)	$CH_3O + NO_2 \rightarrow HCHO + HONO$		$1.5 \cdot 10^{-13}$	[18]
(13)	$CH_3 + NO_2 \rightarrow CH_3O + NO$		$2.5 \cdot 10^{-11}$	[19]
(14)	$HO_2 + NO \rightarrow NO_2 + OH$	$3.7 \cdot 10^{-12} \cdot 10^{104/T}$		[15]
(15)	$OH + NO_2(M) \rightarrow HONO_2$	$1.0 \cdot 10^{-11}$	$1.22 \cdot 10^{-11}$	[15]
(16)	$CH_3O_2 + HO_2 \rightarrow CH_3OOH + O_2$	$1.7 \cdot 10^{-13} \cdot 10^{434/T}$		[15]
(17)	$CH_3O_2 + NO \rightarrow CH_3O + NO_2$	$4.2 \cdot 10^{-12} \cdot 10^{78/T}$		[15]
(18)	$CH_3CO_3 + NO \rightarrow CH_3 + CO_2 + NO_2$	$1.4 \cdot 10^{-11}$		[15]
(19)	$CH_3O + NO \rightarrow CH_3ONO$	$1.9 \cdot 10^{-11}$		[15]
(20)	$CH_3O + NO \rightarrow HCHO + HNO$	$1.3 \cdot 10^{-12}$		[20]
(21)	$PAN + \text{wall} \rightarrow$		$5 \cdot 10^{-5}$	this work
(22)	$CH_3CO_3 + \text{wall} \rightarrow$		0.3	[21]

importance. The values we employed for the wall removal of *PAN* and acetyl peroxy radicals in the 4.5 liter flask were  $4 \cdot 10^{-5} \text{ s}^{-1}$  and  $0.3 \text{ s}^{-1}$ , respectively. These values are in agreement with the experimentally ones determined in an earlier study [21]:  $2 \cdot 10^{-5} \text{ s}^{-1}$  and  $0.3 \text{ s}^{-1}$  (carried out under the same conditions as in the present work).

### *PAN*– $N_2$ System

The major identified decomposition organo-nitrogen product of the system *PAN* in  $N_2$  was methyl nitrate; it constituted  $21 \pm 4\%$  of the initial *PAN* concentration, significantly less than the results of Bruckmann and Willner who found methyl nitrate to constitute 60–75% of the initial *PAN* concentration and also of the results of Senum et al. [6] and Wangberg et al. [7] who accounted almost all nitrogen lost from the *PAN* decomposition as methyl nitrate. We believe that the main reason for our low methyl nitrate yield is that a large part of the methoxy radicals react with oxygen present as impurity in  $N_2$  via reaction (9) instead of  $NO_2$  and reaction (11). Most manufacturers state for  $N_2$  5.0 an  $O_2$  impurity of 3 ppmv. Indeed com-

puter simulations showed that in the absence of  $O_2$  the methyl nitrate yield increases to 71% of the initial *PAN* concentration, not different from the value reported by Bruckmann and Willner. The same simulation also showed that  $NO_2$  continued to be a major product accounting for 21% of initial *PAN* concentration. The yield of methyl nitrite, also measured in the reaction products was less than 0.1% of the initial *PAN* concentration. For an initial *PAN* concentration of 440 ppb the calculated N-mass balance based on the yield of methyl nitrate and remaining *PAN* after 200 min reaction time was only 34%. However, we observed an  $NO_x$  signal of concentration 210 ppb in addition to *PAN* and methyl nitrate. We can speculate on the nature of the product that is responsible for the additional  $NO_x$  signal. From the N-products reported in the literature the excess  $NO_x$  signal can be either  $NO_2$  or nitromethane. If this N-product were nitromethane it would have been detected on the ECD; injections of commercially available compound showed that it elutes at known retention time from the column used. Nitromethane was not observed in our experiments nor did we observe another unidentified peak on the ECD. In addition there is kinetic evidence that excludes the formation of nitromethane. The reaction proposed in previous studies [3, 5, 6] to explain the formation of nitromethane is  $CH_3 + NO_2 \rightarrow CH_3NO_2$ . This reaction is unlikely to occur in our system in the presence of 3 ppm oxygen because of reaction (3). Furthermore, the above reaction is also unlikely to occur in pure *PAN*, because as reported by Yamada et al. [19] it is  $10^4$  times slower (at 1 Torr) than the bimolecular atom transfer reaction  $CH_3 + NO_2 \rightarrow CH_3O + NO$ . Therefore we can safely accept that  $NO_2$ , which does not respond on the ECD, is formed in the *PAN* thermal decomposition in  $N_2$ . The amount of  $NO_2$  formed accounts for 48% of the initial *PAN* concentration and thus raises the N-mass balance to 82%. From the past studies only Bruckmann and Willner observed the formation of  $NO_2$  in the pure *PAN* decomposition, but unfortunately no comparison can be made because they did not report quantitative ratios of both  $NO_2$  and methyl nitrate.

The experimental results with the best computer simulation of the *PAN*- $N_2$  system is shown in Fig. 1. Two cases were examined in the simulation. First the free radical only mechanism; this case yielded the worst simulation. The second case in addition to the free radical reaction scheme included the heterogeneous removal of *PAN* and acetyl peroxy radicals. The introduction of the wall removal

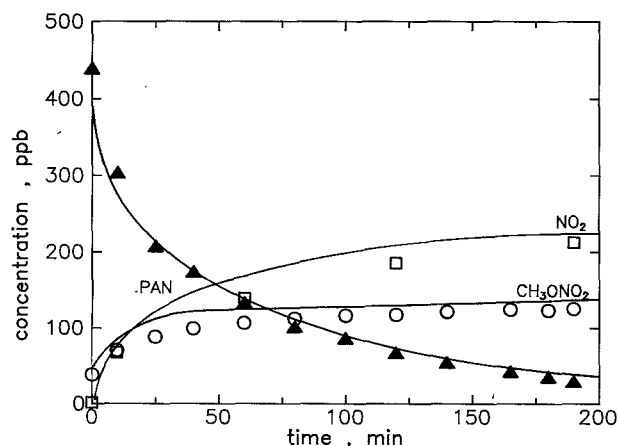


Fig. 1. Time profiles of pure *PAN*, methyl nitrate and  $NO_2$  at  $50^\circ C$ ; experimental points: *PAN*  $\blacktriangle$ ,  $CH_3ONO_2$   $\circ$ ,  $NO_2$   $\square$ ; Simulation: \_\_\_\_\_

of acetyl peroxy radical via reaction (22) in the mechanism resulted in a decreased rate of *PAN* destruction and also allowed the formation of  $\text{NO}_2$ , and thus simulated very well the experimentally determined *PAN*, methyl nitrate, and  $\text{NO}_2$  profiles. Kinetic simulations showed that the initial concentration of acetyl peroxy radicals after the introduction of reaction (22) was reduced 2.3 times. A result of this  $\text{CH}_3\text{COO}_2$  decrease was the reduction of the rates of the very important reaction (2) as well as (7) and (8) and consequently the overall decrease of the *PAN* decay rate and it was more pronounced in the early stages of the reaction. If we included in the simulation scheme the concerted reaction:  $\text{PAN} \rightarrow \text{CH}_3\text{ONO}_2 + \text{CO}_2$  with the rate constant given by Senum et al. [6]  $k = 2.1 \cdot 10^{12} \cdot 10^{-5419/T}$ , then the *PAN* profile became too steep, the methyl nitrate increased more above the experimental points whereas the  $\text{NO}_2$  remained unaffected.

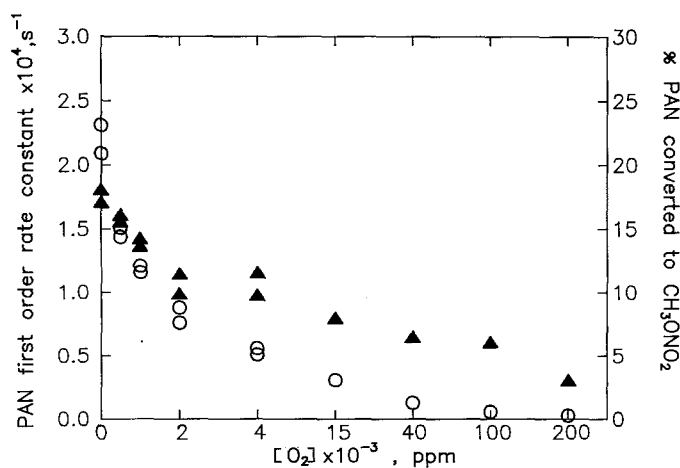
### *PAN*– $\text{O}_2$ System

An argument in favour of the free radical and heterogeneous *PAN* decay and against the Senum et al. homolytic decomposition was the results in the presence of added oxygen. As shown in Fig. 2 the methyl nitrate yield decreased with increasing the  $\text{O}_2$  concentration, ending up with zero methyl nitrate formation when  $[\text{O}_2] > 40\,000$  ppm at  $50^\circ\text{C}$ . If there existed a homolytic path to methyl nitrate and carbon dioxide we ought to have always obtained methyl nitrate. In the free radical mechanism however the methoxy radicals, formed mostly from the methyl peroxy radicals, reaction (4), and less from reaction (13) of the methyl radicals with  $\text{NO}_2$ , are expected on the basis of the free radical mechanism to react either with  $\text{NO}_2$ :  $\text{CH}_3\text{O} + \text{NO}_2 \rightarrow \text{CH}_3\text{ONO}_2$  (11), or with  $\text{O}_2$ :  $\text{CH}_3\text{O} + \text{O}_2 \rightarrow \text{HCHO} + \text{HO}_2$  (9)

The reaction



is 100 times slower than reaction (11) and would not contribute significantly. The



**Fig. 2.** Effect of added oxygen on the *PAN* decay rate and the methyl nitrate formed;  $50^\circ\text{C}$ , initial *PAN* concentration 320–400 ppb; *PAN* ▲,  $\text{CH}_3\text{ONO}_2$  ○

rate constants favour reaction (11) over reaction (9) by an order of  $10^4$ , but at sufficiently large  $[O_2]$  the methyl nitrate yield would decrease to zero.

The decrease of the *PAN* decay rate after the addition of  $O_2$  (also shown in Fig. 2) can also be explained in terms of the free radical only mechanism. Oxygen removes the methoxy radicals via reaction (9) and thus the main route of removal of  $NO_2$  via reaction (11) is limited. Therefore, the  $NO_2$  concentration increases and stabilizes *PAN* via reaction (-1). FACSIMILE simulations showed that indeed the  $NO_2$  concentration increases as the added  $O_2$  increases.

### *PAN*– $NO_2$ System

The purpose of these experiments was to suppress the decay of *PAN* via reaction (-1) with the addition of large amounts of  $NO_2$  and thus allowing the homolytic decay to methyl nitrate and carbon dioxide if this exists. However, as shown in Fig. 3 this was not observed experimentally. The *PAN* decay rate was indeed diminishing up to a minimum at added  $[NO_2]=2.4$  ppm along with the yield of methyl nitrate. Further addition of  $NO_2$  increased the *PAN* decay rate and the methyl nitrate yield. This behaviour was also recently reported by Wangberg et al. [7] who offered no explanation. We believe that the increased *PAN* decay rate is due to  $NO$  which we found experimentally to be present in the system at initial concentrations equal to 1.3% of the added  $NO_2$ . Although the competition between the stabilizing reaction (-1) and destabilizing reaction (18) is in favour of reaction (-1) mainly because of the small concentration of  $NO$ , still at high  $NO_2$  there will be enough  $NO$  (compared to *PAN*) to enhance all the reactions of Table 1 involving  $NO$  and thus leading to increased *PAN* decay rates. Higher methyl nitrate yields are also expected from the free radical reaction scheme, because at large  $NO_2$  concentrations reaction (11) becomes more significant compared to reaction (9) and thus leads to more methyl nitrate.

This explanation based on the presence of  $NO$  was corroborated by the results of FACSIMILE simulations employing the free radical mechanism with the het-

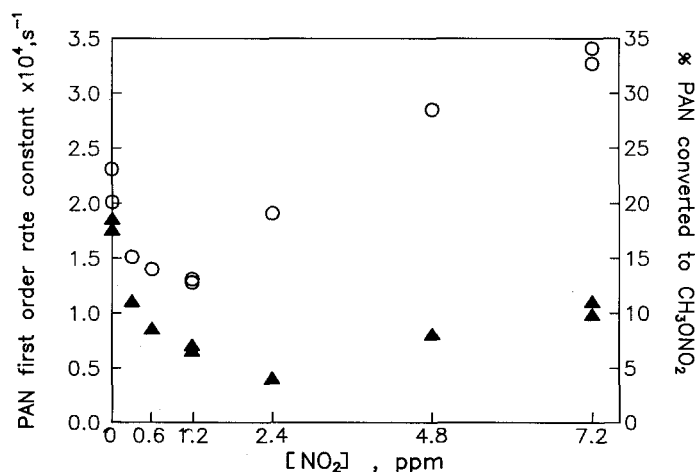


Fig. 3. Effect of added  $NO_2$  on the *PAN* decay rate and on the methyl nitrate formed; 50°C, initial *PAN* concentration 300–400 ppb; *PAN* ▲,  $CH_3ONO_2$  ○

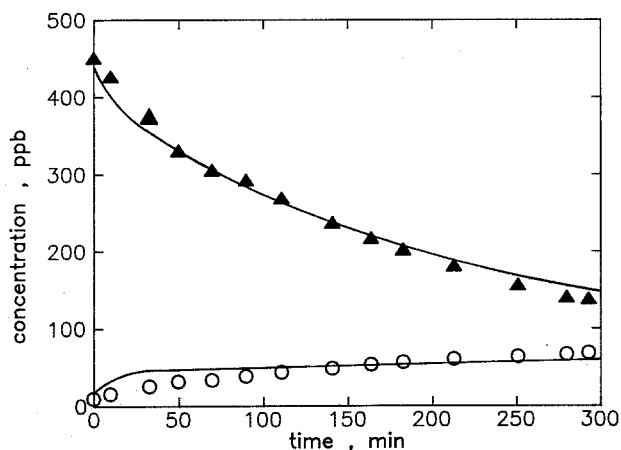


Fig. 4. Time profiles of *PAN* and methyl nitrate in the presence of 1 200 ppb  $\text{NO}_2$  at  $50^\circ\text{C}$ ; experimental points: *PAN*  $\blacktriangle$   $\text{CH}_3\text{ONO}_2$   $\circ$ ; simulation: —

erogeneous contribution (shown in Fig. 4). If  $\text{NO}$  was not included in the initiating part of the program the resulting simulations (not shown) were very poor. There was no reason to examine the homolytic pathway reported by Senum et al. [6] because the amount of methyl nitrate formed in the simulation was in agreement with the experimentally measured one. It must be pointed out that the  $\text{O}_2$  concentration employed in this simulation was 14 ppm. This value can be obtained if we recall that  $\text{NO}_2$  was made from an  $[\text{O}_2]/[\text{NO}]$  ratio of 9 : 1. Therefore, introduction of 1 200 ppb  $\text{NO}_2$  means the simultaneous introduction of 11 ppm  $\text{O}_2$  thus making the total  $[\text{O}_2] = 14$  ppm.

#### *PAN*– $\text{NO}$ System

The reaction of *PAN* with  $\text{NO}$  is of great interest because it enhances the *PAN* decay, and also in the presence of large excess  $\text{NO}$  the measured *PAN* decay rate equals the rate of reaction (1). The first order rate constant for reaction (1) that we obtained at  $23.5^\circ\text{C}$  in the 425 l reaction vessel was  $3.1 \cdot 10^{-4} \text{ s}^{-1}$  (cf. the plateau

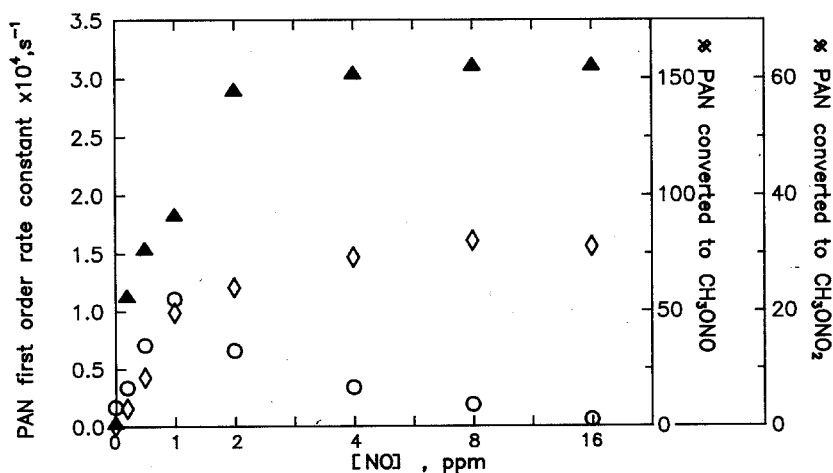


Fig. 5. Effect of added  $\text{NO}$  on the *PAN* decay rate and on methyl nitrate and methyl nitrite formed;  $23.5^\circ\text{C}$ , initial *PAN* concentration 350–400 ppb; *PAN*  $\blacktriangle$ ,  $\text{CH}_3\text{ONO}_2$   $\circ$ ,  $\text{CH}_3\text{ONO}$   $\diamond$



region in Fig. 5) whereas in the 4.51 flask  $3.4 \cdot 10^{-4} \text{ s}^{-1}$ . The experimental uncertainty accounts for the 10% difference as indicated from  $2\sigma = 0.60$  obtained for the experiments carried out in the small reaction vessel. The value  $3.1 \cdot 10^{-4} \text{ s}^{-1}$  is the same as the value reported by Niki et al. [22] and very close to the value  $2.83 \cdot 10^{-4} \text{ s}^{-1}$  reported by Pate et al. [8] but significantly larger than the corresponding values of  $2.2 \cdot 10^{-4} \text{ s}^{-1}$  and  $1.73 \cdot 10^{-4} \text{ s}^{-1}$  reported by Senum et al. [6] and Wangberg et al. [7], respectively, and approximately 30% lower than the values reported by Schurath and Wipprecht [14], Hendry and Kenly [4], and Cox and Roffey [3].

The major product of these experiments was  $\text{NO}_2$ . The yield of  $\text{NO}_2$  relative to the change of the *PAN* concentration was  $1.7 \pm 0.3$ . Simultaneously the  $\Delta[\text{NO}]/\Delta[\text{PAN}]$  observed was  $2.7 \pm 0.4$ . One could visualize the formation of one mol of  $\text{NO}_2$  to result from reaction (1):  $\text{PAN} \rightarrow \text{CH}_3\text{COO}_2 + \text{NO}_2$  and one mol from reaction (18):  $\text{CH}_3\text{COO}_2 + \text{NO} \rightarrow \text{CH}_3\text{CO}_2 + \text{NO}_2$ . Under these conditions one mol of  $\text{NO}$  would disappear per mol of reacting *PAN*, due to reaction (19), because the obtained yield of methyl nitrite versus *PAN* consumed is close to unity. The remaining almost two mol of consumed  $\text{NO}$  per mol of reacting *PAN* would be due to reactions (18), (17), and (14).

In contrast to earlier studies [6–8] these experiments showed that the major organo-nitrogen product was methyl nitrite and not methyl nitrate. When a large excess of  $\text{NO}$  was added the methyl nitrite constituted 75% of the initial *PAN* concentration. Formation of this product, when  $\text{NO}$  is in large excess, is entirely reasonable to result from reaction (19):  $\text{CH}_3\text{O} + \text{NO} \rightarrow \text{CH}_3\text{ONO}$  and surpass methyl nitrate formed via reaction (11):  $\text{CH}_3\text{O} + \text{NO}_2 \rightarrow \text{CH}_3\text{ONO}_2$ . In fact, for added  $[\text{NO}] > 8$  ppm methyl nitrate was not formed at all. Earlier studies reported methyl nitrite to be a minor product when compared to methyl nitrate [8] whereas others did not observe it at all [6, 7]. The obtained profile of methyl nitrate formed vs. added  $\text{NO}$  (Fig. 5) shows that its formation depends on the *PAN* and  $\text{NO}$  concentrations employed and this explains the results of Wangberg et al. who reported formation of no methyl nitrate, and also the results of Senum et al. who reported formation of methyl nitrate. Presumably the last mentioned authors did not employ

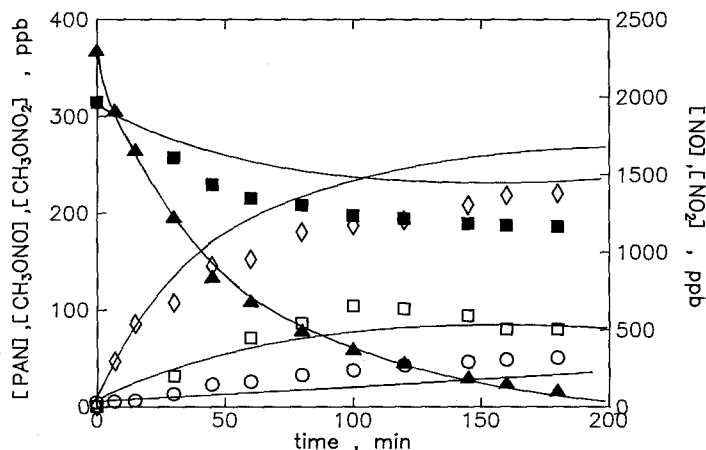


Fig. 6. Time profiles of *PAN* and methyl nitrate in the presence of 2 ppb  $\text{NO}$  at  $23.5^\circ\text{C}$ ; experimental points: *PAN*  $\blacktriangle$ ,  $\text{CH}_3\text{ONO}_2$   $\circ$ ,  $\text{CH}_3\text{ONO}$   $\diamond$ ,  $\text{NO}$   $\blacksquare$ ,  $\text{NO}_2$   $\square$ ; simulation: —

a high enough  $[\text{NO}]/[\text{PAN}]$  ratio and thus they obtained methyl nitrate. The simulation and experimental results of the system  $\text{PAN} + \text{NO}$  in  $\text{N}_2$  are shown in Fig. 6. There was no point in testing the contribution of the homolytic pathway, because at  $23.5^\circ\text{C}$  the rate constant reported by Senum et al. is only  $1 \cdot 10^{-6} \text{ s}^{-1}$  and would therefore contribute negligible amounts of methyl nitrate. In addition, as seen in Fig. 5, the methyl nitrate formed diminishes towards zero at high NO concentrations. Again the reaction scheme employed in the computer simulations is the one shown in Table 1. PAN and methyl nitrate were very well simulated, NO and  $\text{NO}_2$  were acceptable in view of their large experimental uncertainties, while methyl nitrite is more than experimentally observed. The ratios of  $\Delta[\text{NO}_2]/\Delta[\text{PAN}]$  and  $\Delta[\text{NO}]/\Delta[\text{PAN}]$  obtained from the simulations were 1.5 and 2.4 respectively, in good agreement with the experimentally determined values.

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